



Experimental and numerical simulation of restarting flow of gelled crude oil.

Multiphase 2017 – ENS Paris-Saclay (Cachan, France)

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18/10/2017

Wax is the challenge!

- What is wax?
- Wax is...
- ...something you know:

(one particular form of wax,
however...)

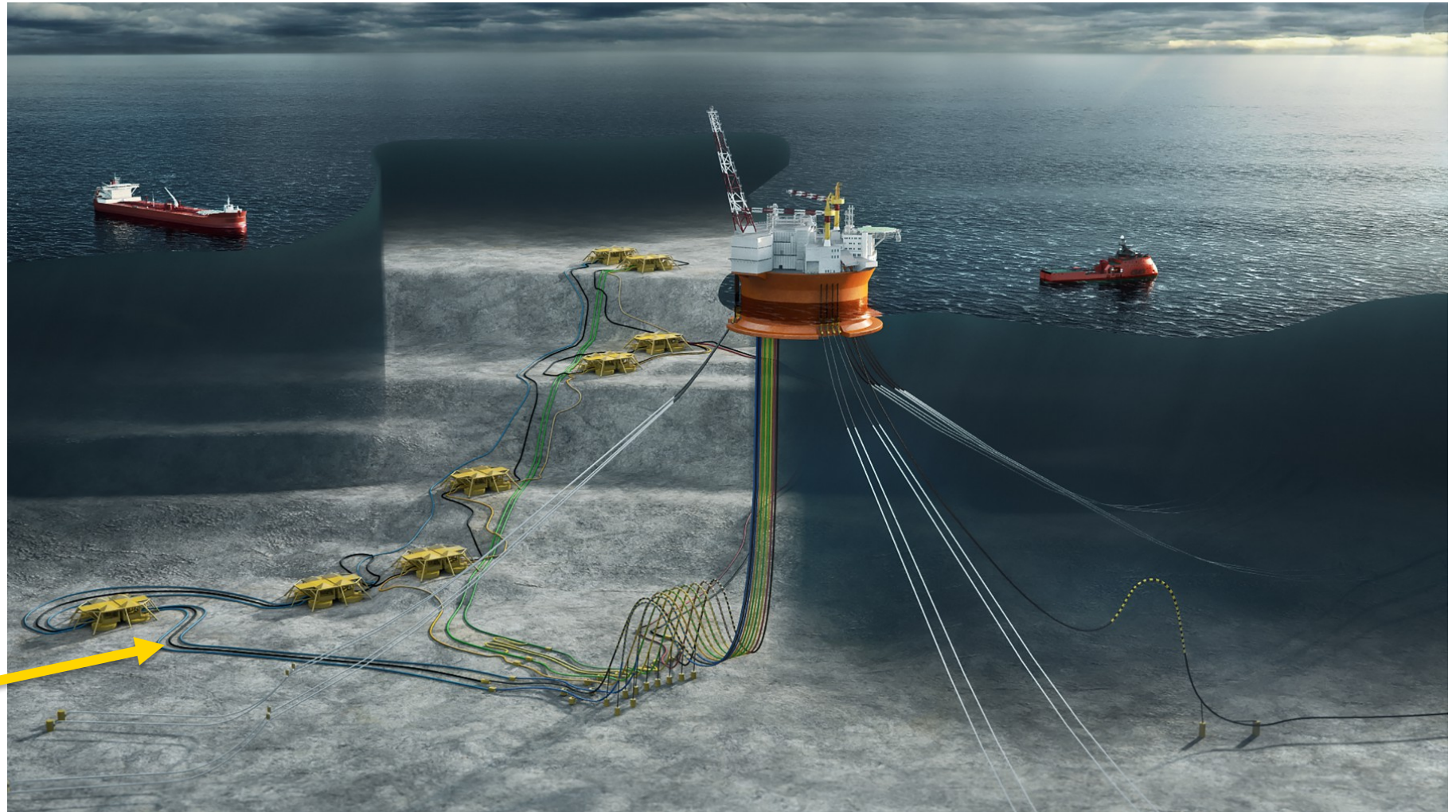


Foto:
<https://en.wikipedia.org/wiki/Candle>

Where may we find wax?

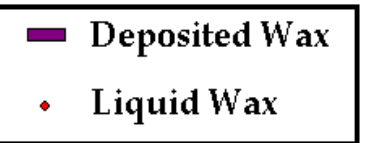
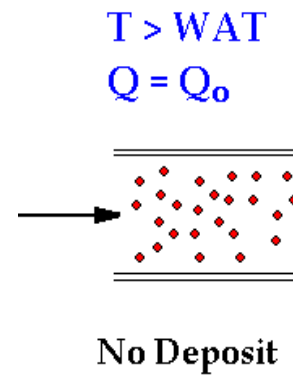
- In every cold or subsea development there is RISK of wax deposition
- This risk must be taken into account during equipment design

(e.g. in pipelines)



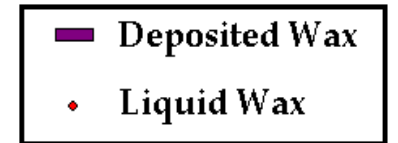
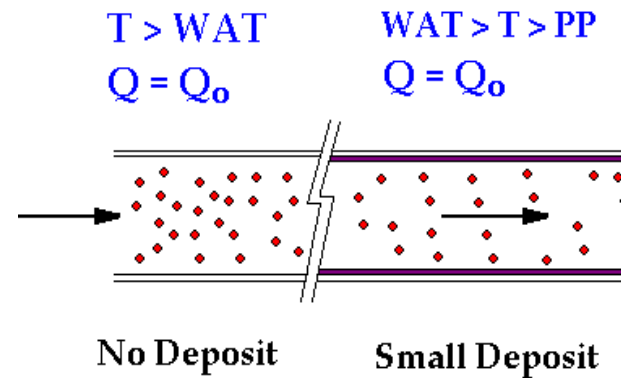
What happens in the pipeline transporting waxy crudes?

- Crude oil flows into the pipeline, temperature is high.



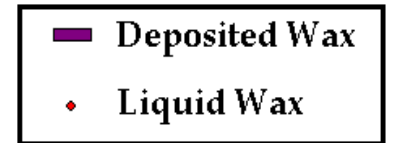
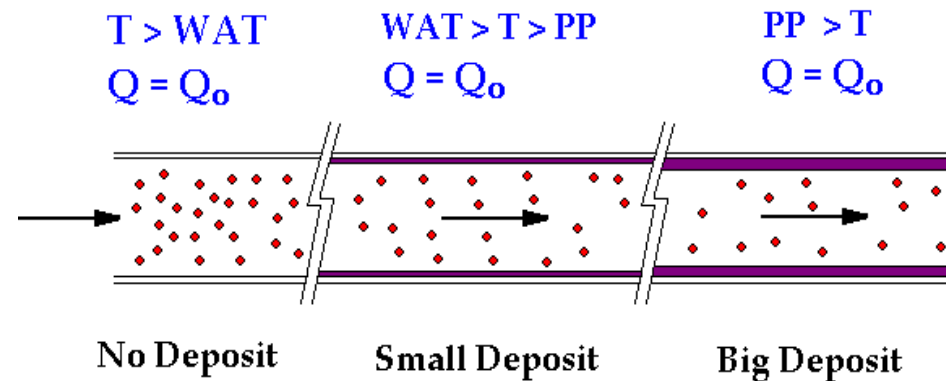
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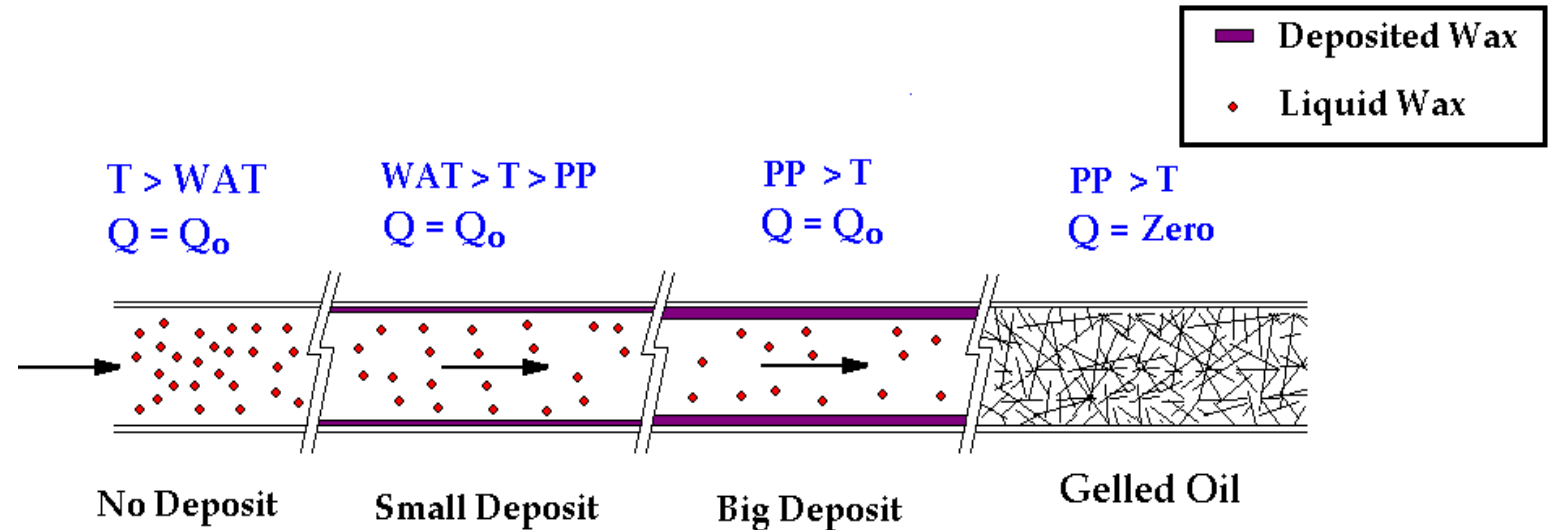
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What happens in the pipeline transporting waxy crudes?

- Crude oil flows into the pipeline, temperature is high.
- Pipeline is cooled by the sea, temperature lower than WAT.
- Wax precipitates and may deposit on pipe inner wall.
- Eventually the fluid forms a gel and flow is blocked.



How to study wax?

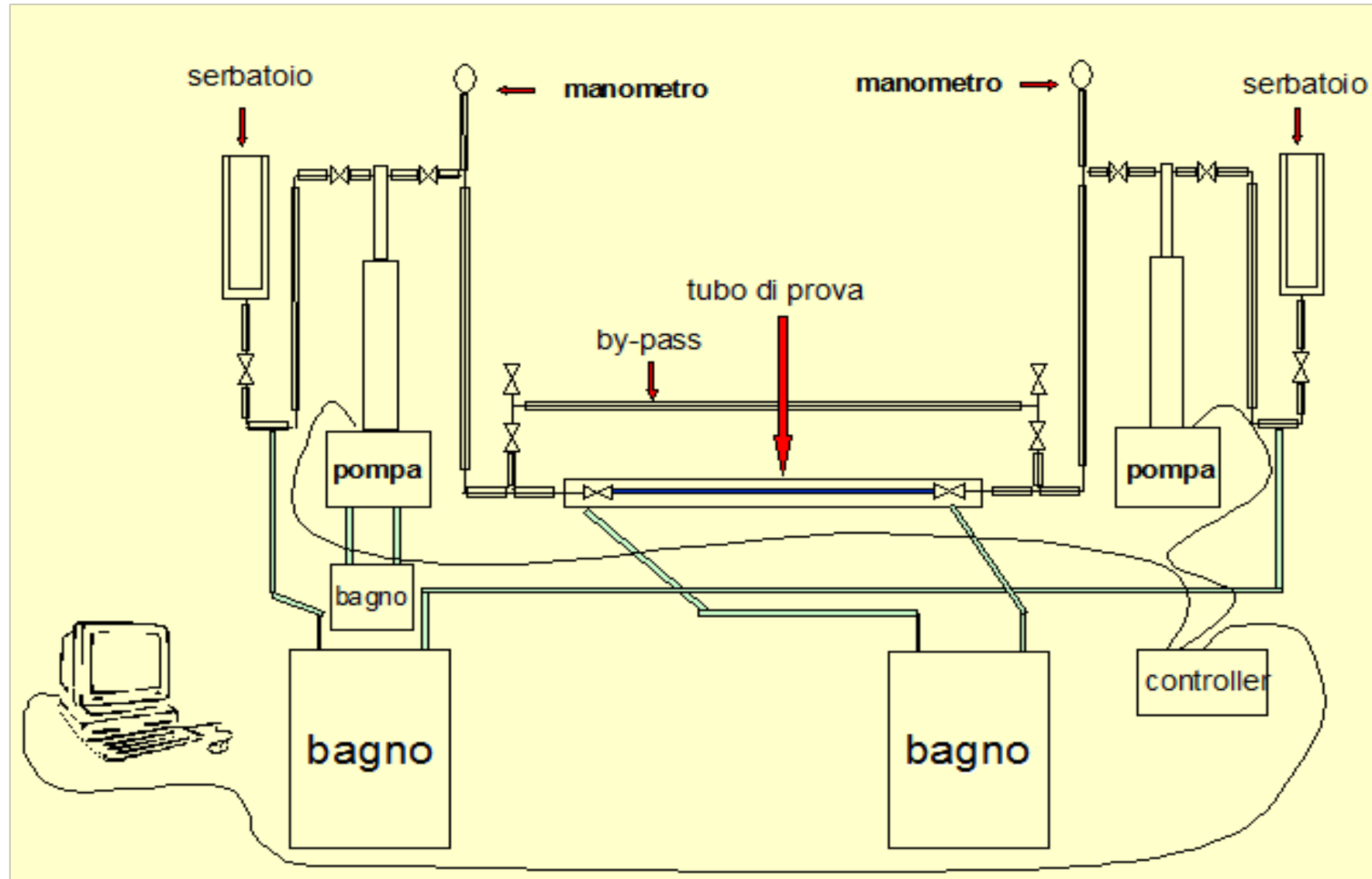
Move to controlled settings. Go to the lab...

The lab.

A picture from one of our lab buildings.

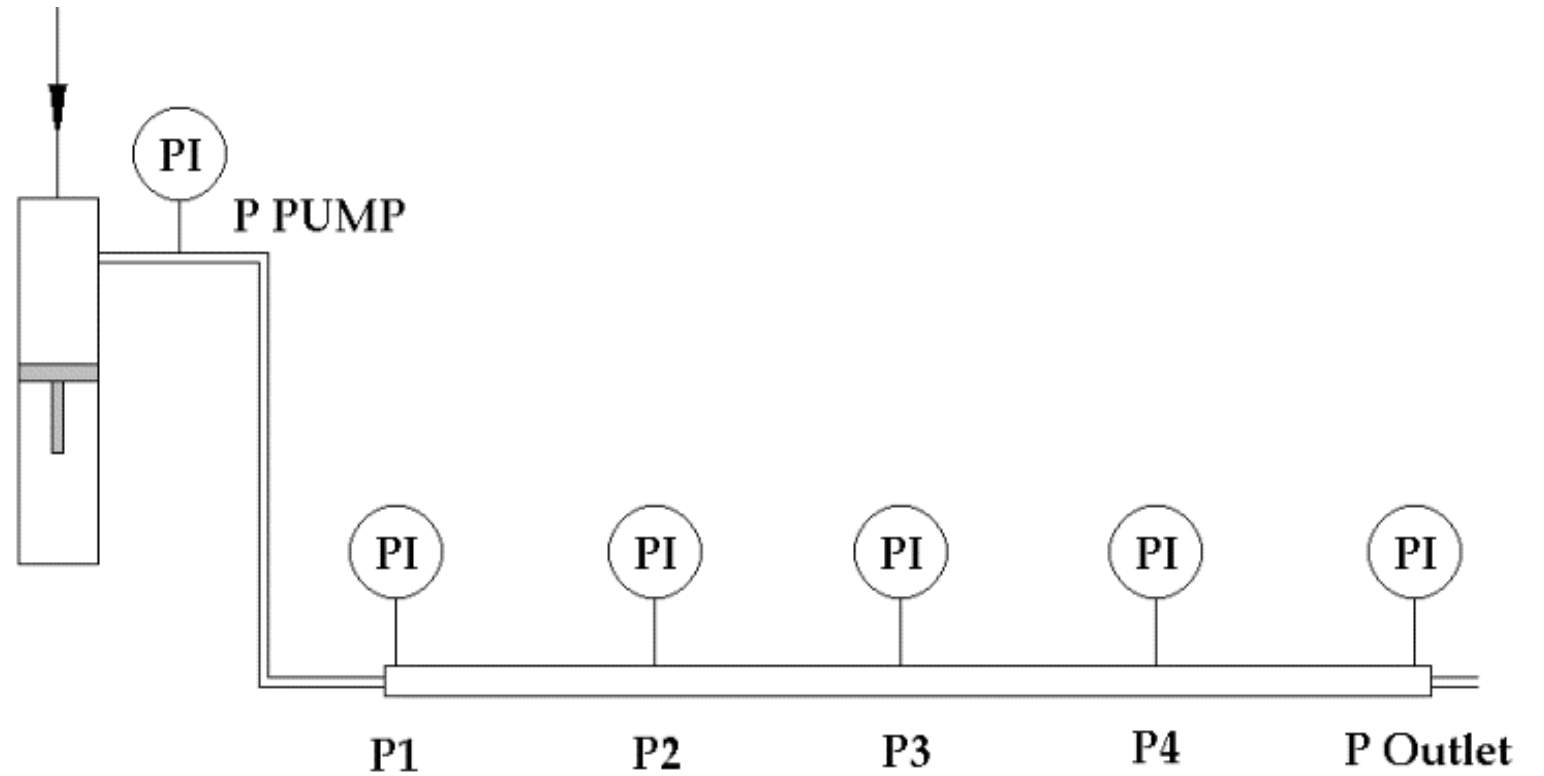


The lab – sketch of apparatus



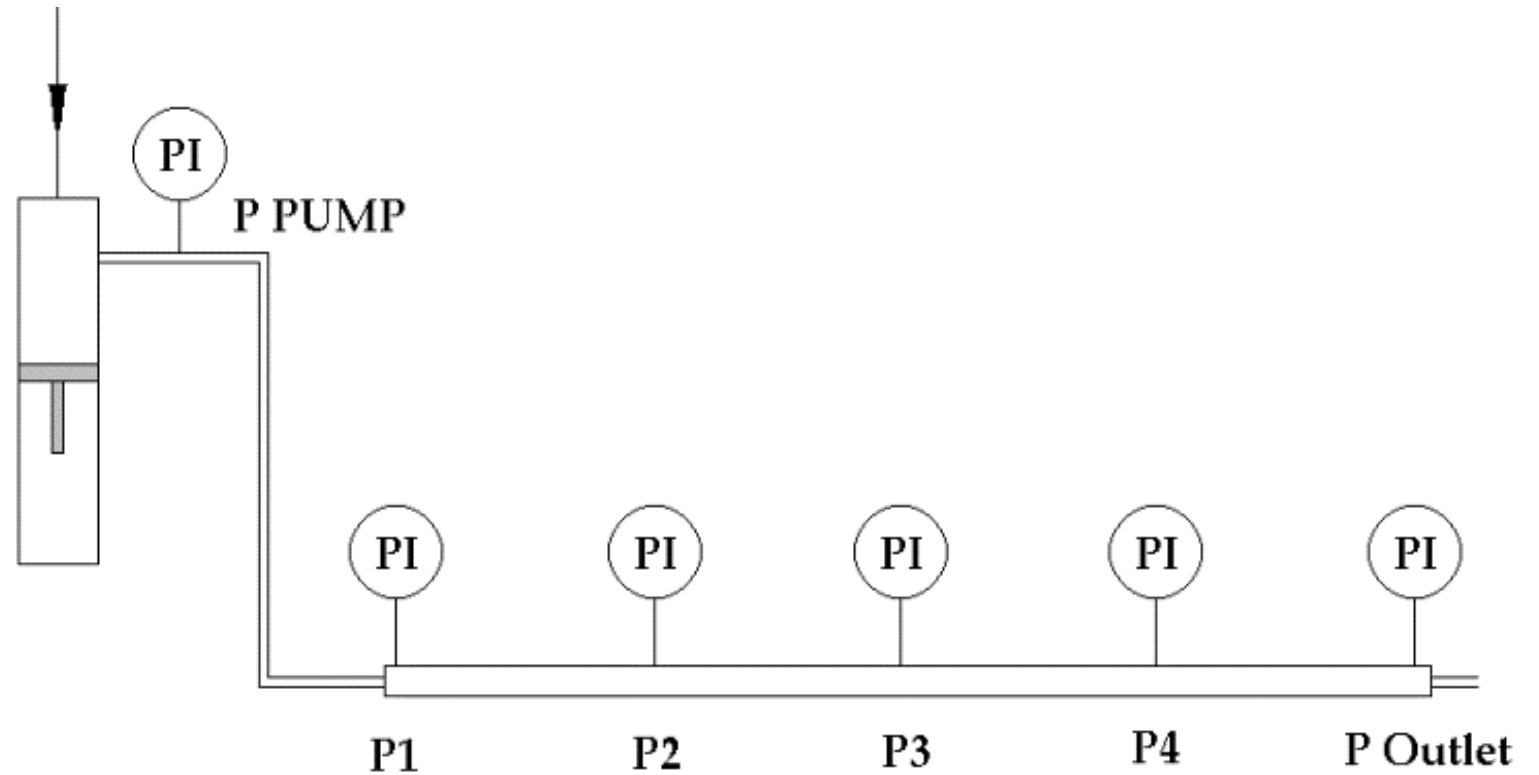
The lab – the working principle.

- Step 1: Pipes are filled with crude oil.



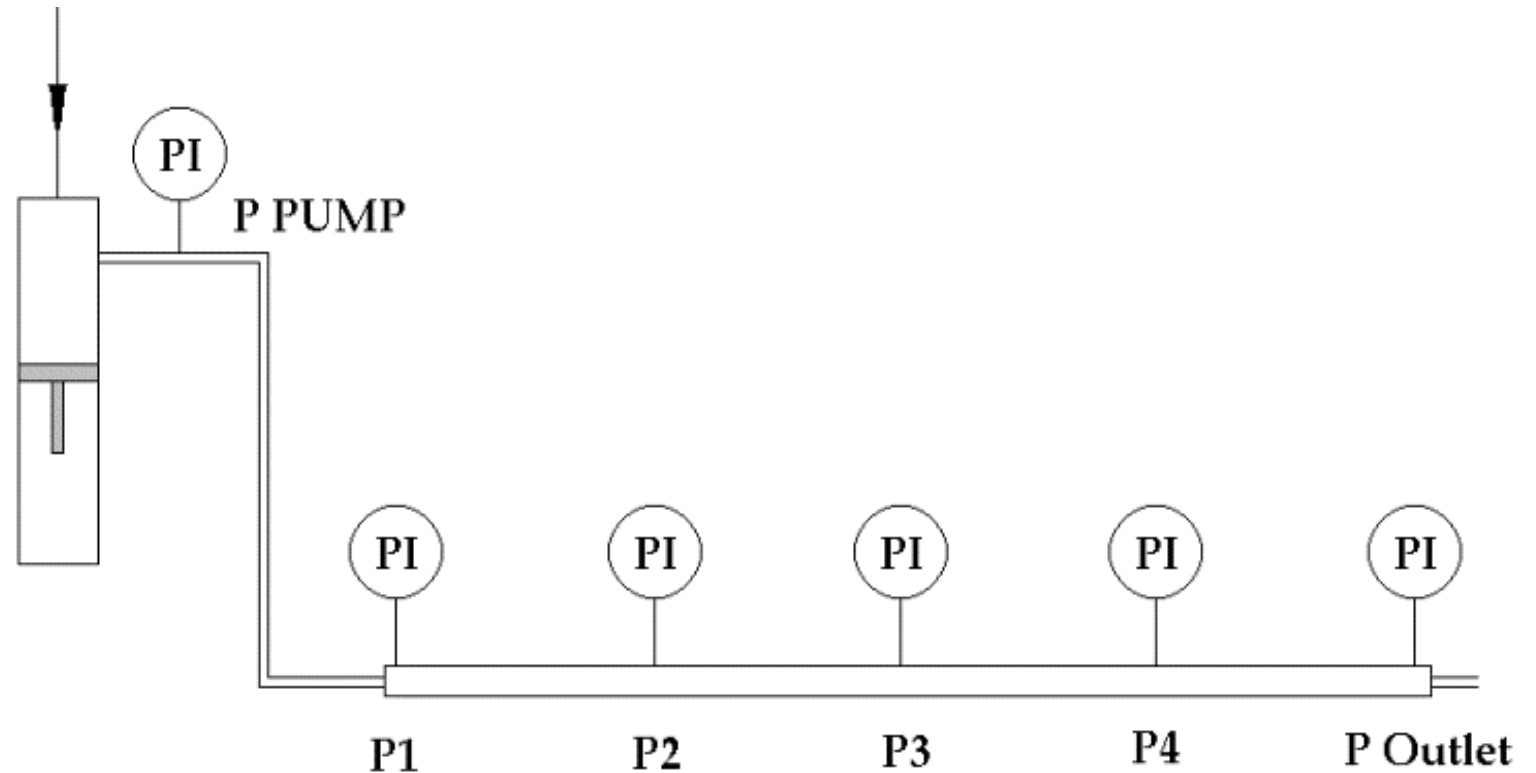
The lab – the working principle.

- Step 1: Pipes are filled with crude oil.
- Step 2: Temperature of piping is controlled by cooling equipment.



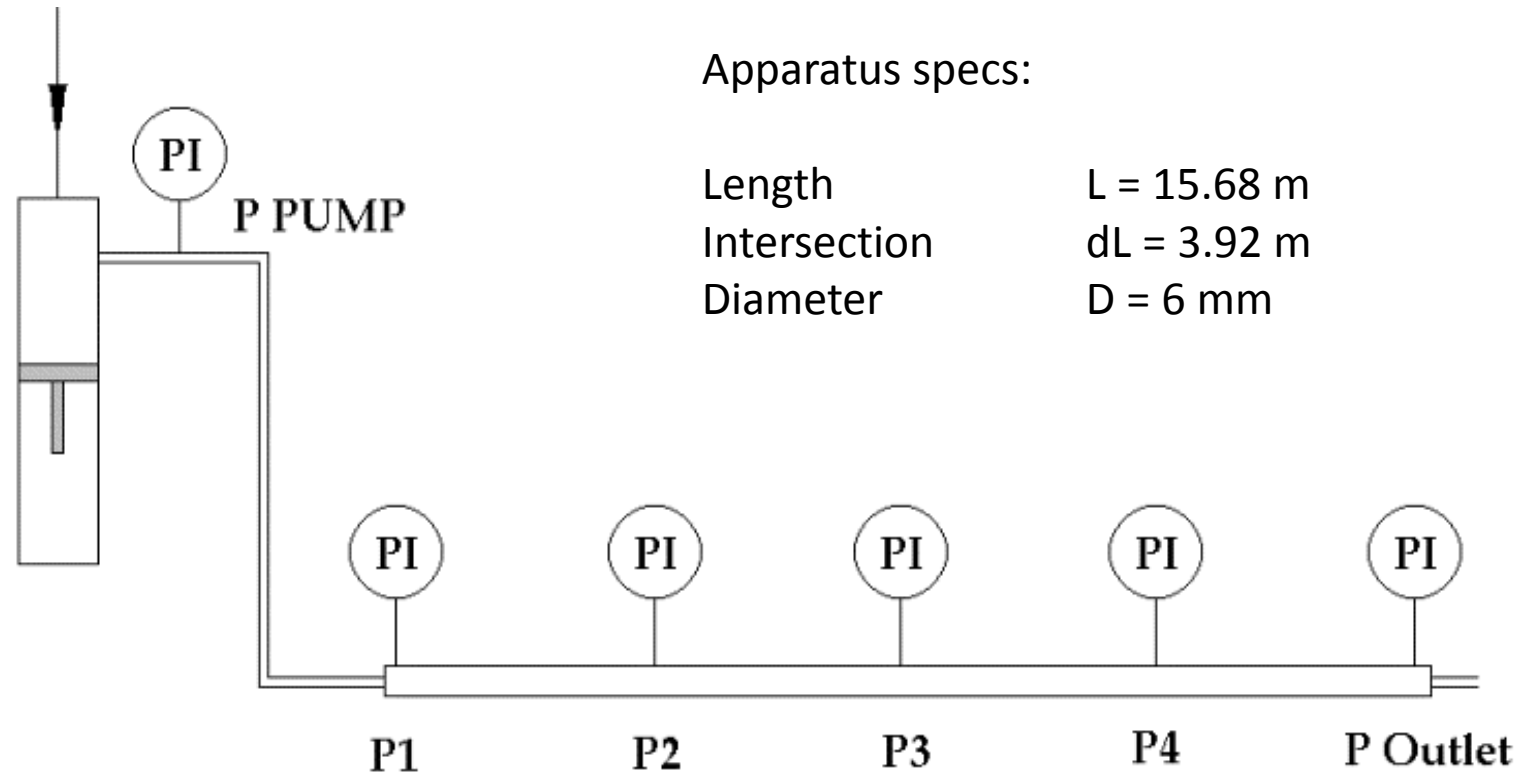
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- Step 1: Pipes are filled with crude oil.
- Step 2: Temperature of piping is controlled by cooling equipment.
- Step 3: Pump is activated delivering fresh fluid pushing the gel towards outlet.



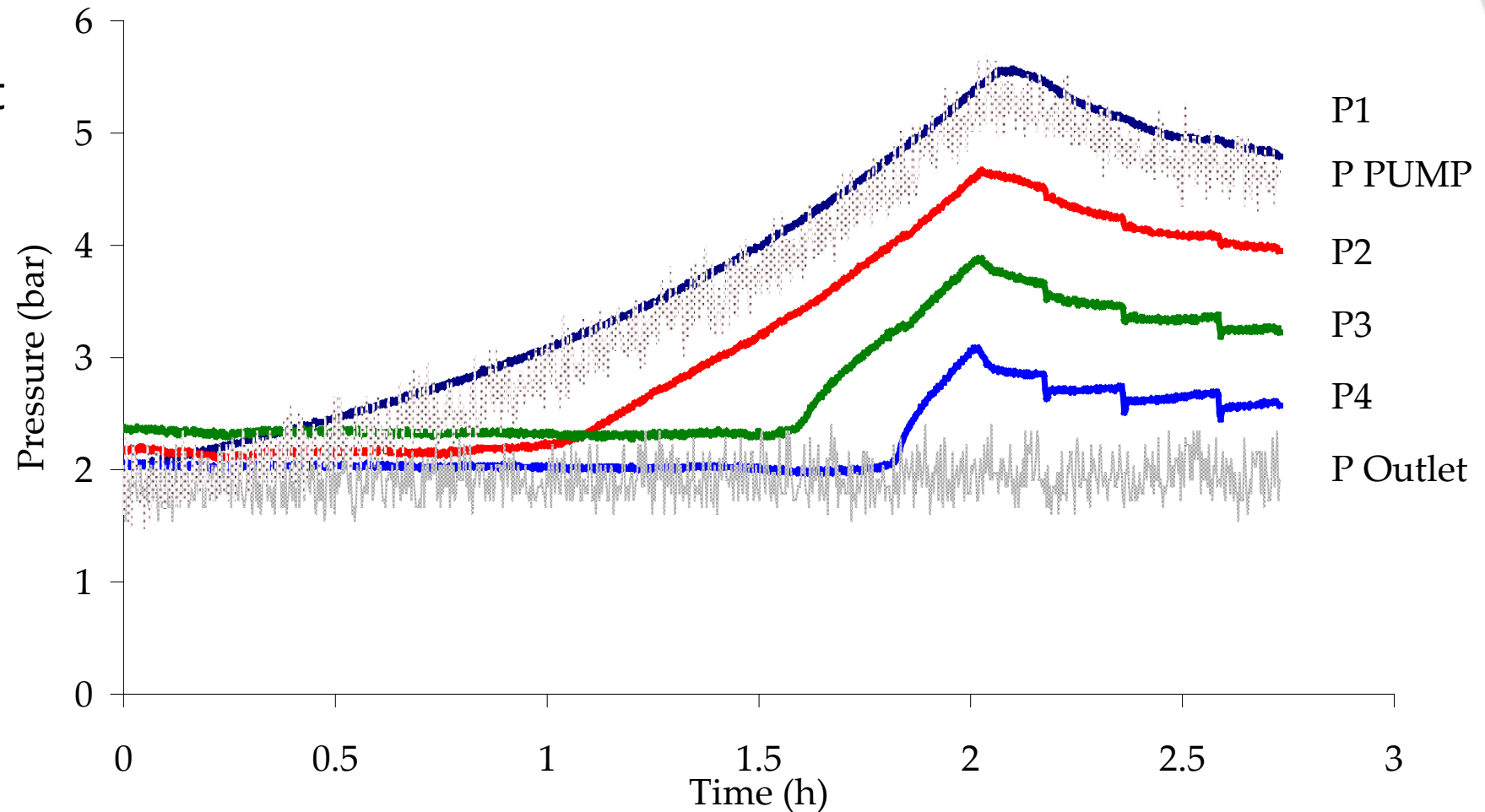
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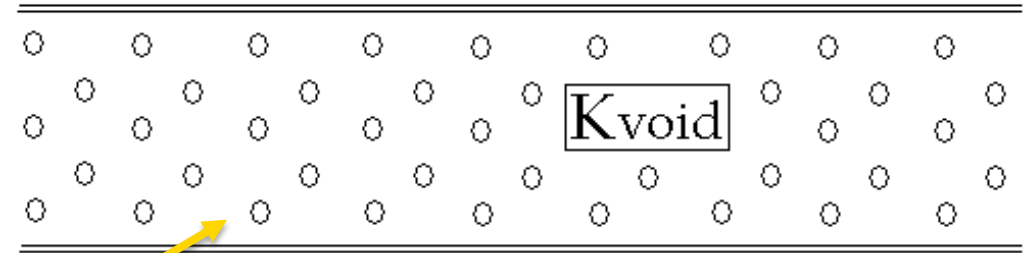
The lab – outcome.

- Pressure is monitored at 5 positions during time.
- Notice clouds of points:
 - P PUMP
 - P Outlet
- Notice blue line P4:
 - Avalanches after peak
- Pressure-peak after 2h:
 - i.e. gel starts to move



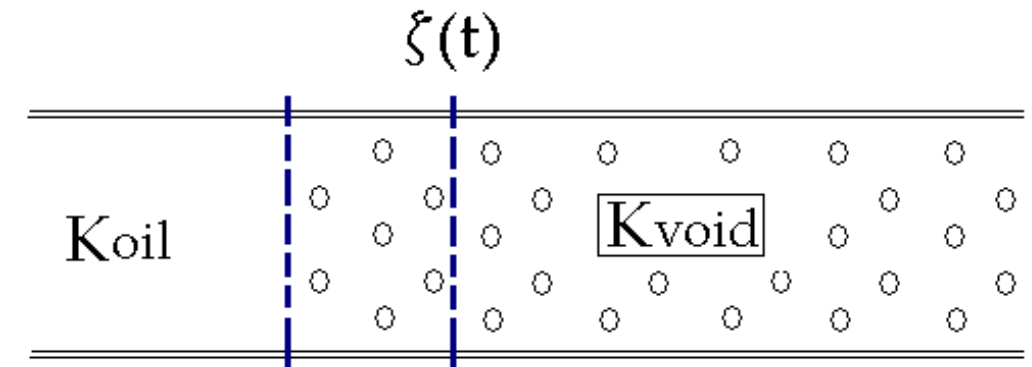
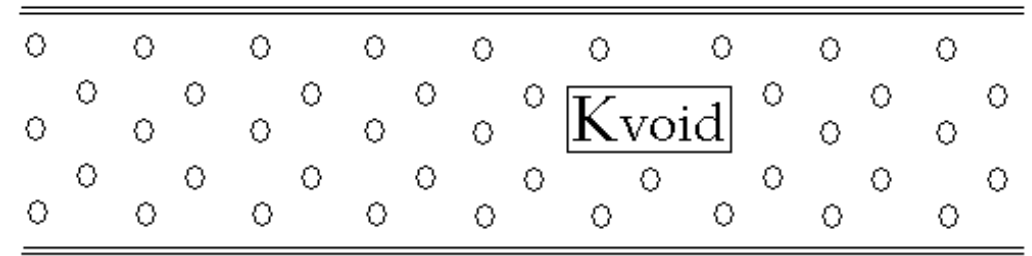
The lab – multiphase conditions.

- As before, the cold waxy gel is formed.
 - Phase transition takes place.
- In case of longer time without flow:
 - Ageing of gel
 - The gel becomes more compact
 - Volume change due to solidification
 - Voids start to appear
 - Hence: Non-Newton liquid + solids + gas pockets



The lab – multiphase conditions.

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- In case of longer time without flow:
 - Ageing of gel
 - The gel becomes more compact
 - Volume change due to solidification
 - Voids start to appear
 - Hence: Non-Newton liquid + solids + gas pockets
- Restart of flow:
 - Push gel mixture with oil.
 - Pressure and stress act in a interface ZONE
 - Beyond the ZONE no pressure change appears



$\xi(t-dt)$

How to model wax?

Start with a model from literature...

[Startup flow of gelled crudes in pipelines; de Souza Mendes et. Al.; Journal of Non-Newtonian Fluid Mechanics; 2012]

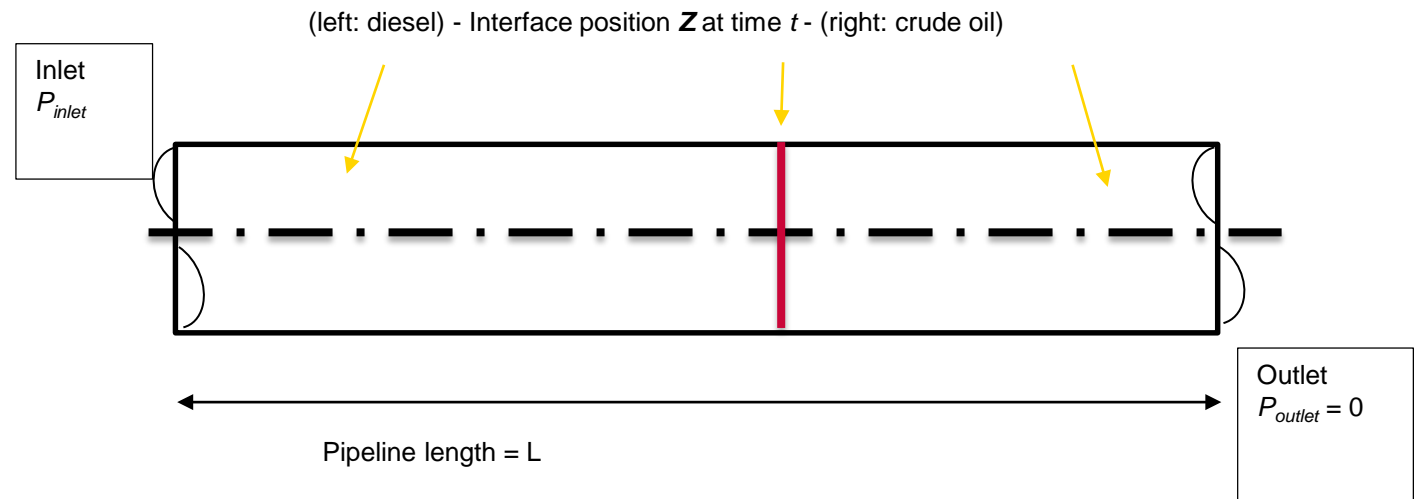


Modelling of pipe.

The numerical model of production-restart is limited to:

- -only the flow inside the pipeline
- -other parts of production facilities are excluded
- -e.g. valves
- -e.g. separators, etc.

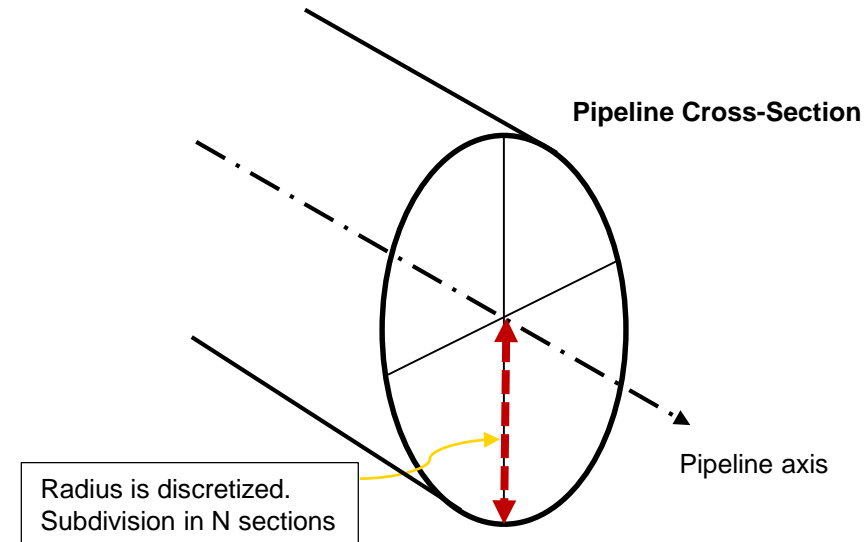
Consists of two fluid lumps.



Modelling of fluid.

As proposed in paper:

- Interface between a Newtonian and a NON-Newtonian is tracked.
- The NON-Newtonian fluid is modelled with a Thixotropic behaviour.
- Velocity profile and Structure-Function is modelled on cross-section.



A very simple model indeed.

Newtonian equations and structure function.

Position of interface between fluids 'Z':

$$\frac{dz}{dt} = \bar{U}(t)$$

Newtons law:

$$\begin{aligned} & (\rho_{diesel}z + \rho_{crude}(L - z)) \frac{d\bar{U}}{dt} \\ & = P_e - \frac{2}{R} (\tau_{diesel}z + \tau_{crude}(L - z)) \end{aligned}$$

The structure parameter lambda.

In general it is a function of both stress and also time.

When $\lambda=1.0$ then the fluid is with max structure, i.e. implicates largest possible viscosity (a gel).

When $\lambda=0.0$ the viscosity is at minimum.

$$\lambda = \lambda(\tau, t)$$



Equation set for thixotropic model.

Viscosity function:

$$\eta(\lambda) = \left(\frac{\eta_0}{\eta_\infty}\right)^\lambda \eta_\infty$$

Stress equation:

$$\tau = \eta_{eq}(\dot{\gamma}_{eq})\dot{\gamma}_{eq}$$

Viscosity function for viscoplastic materials:

$$\eta_{eq}(\dot{\gamma}_{eq}) = \left[1 - e\left(-\frac{\eta_0\dot{\gamma}_{eq}}{\tau_0}\right)\right] \left\{\frac{\tau_0}{\dot{\gamma}} + K\dot{\gamma}_{eq}^{n-1}\right\} + \eta_\infty$$

Structure function:

$$\frac{d\lambda}{dt} = \frac{1}{t_{eq}} \left[(1 - \lambda)^a - (1 - \lambda_{eq}(\tau))^a \left(\frac{\lambda}{\lambda_{eq}(\tau)}\right)^b \right]$$

Deformation rate becomes shear rate:

$$\dot{\gamma}(r, t) = -\frac{\partial v_z}{\partial r}(r, t)$$

Simple mean velocity and -profile relation:

$$\bar{U}(t) = \frac{1}{\pi R^2} \int_0^R 2\pi r v dr$$



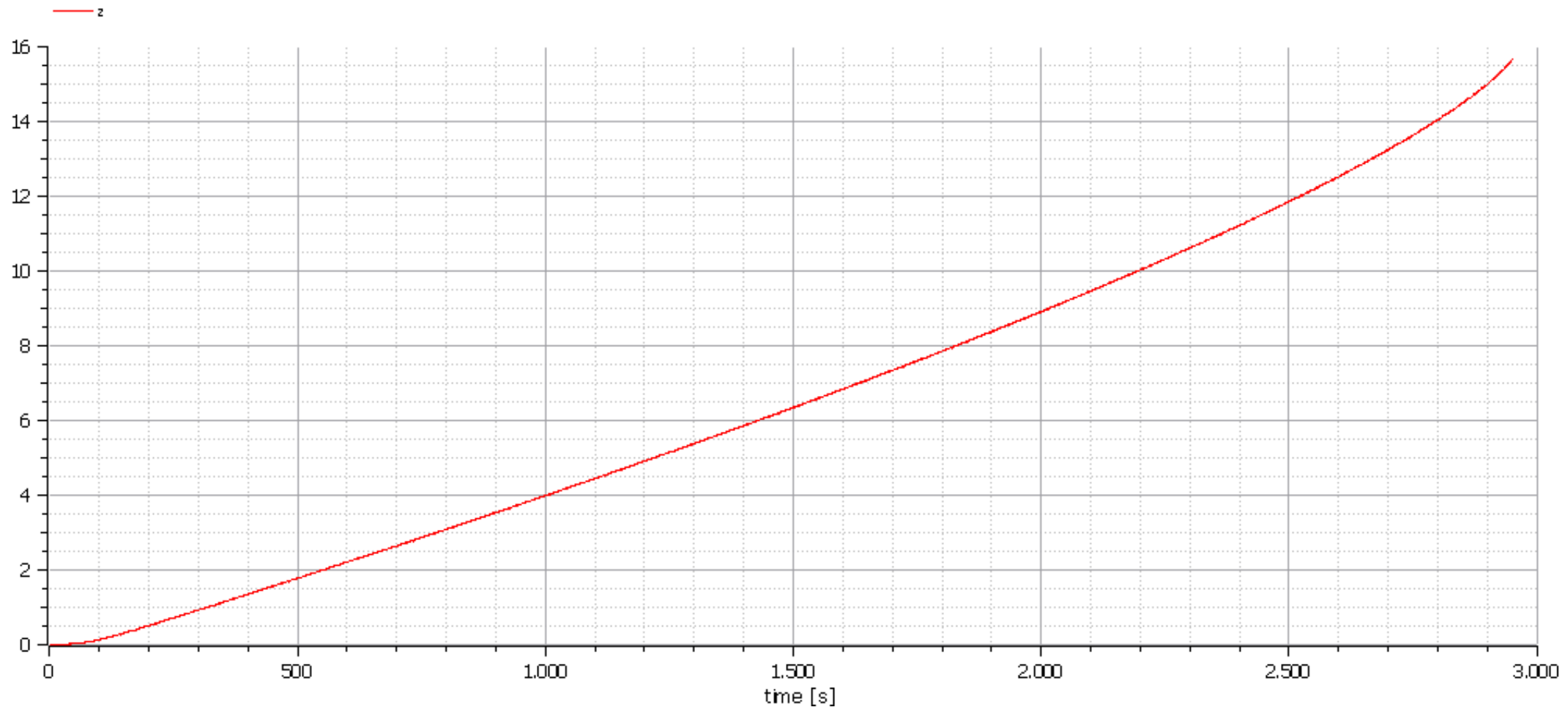
Tuning the thixotropic model.

- A two step procedure.
- Of course begin with DATA set inserted and a start to iterate...
- ...search for adequate numerical values of tuning parameters

DATA

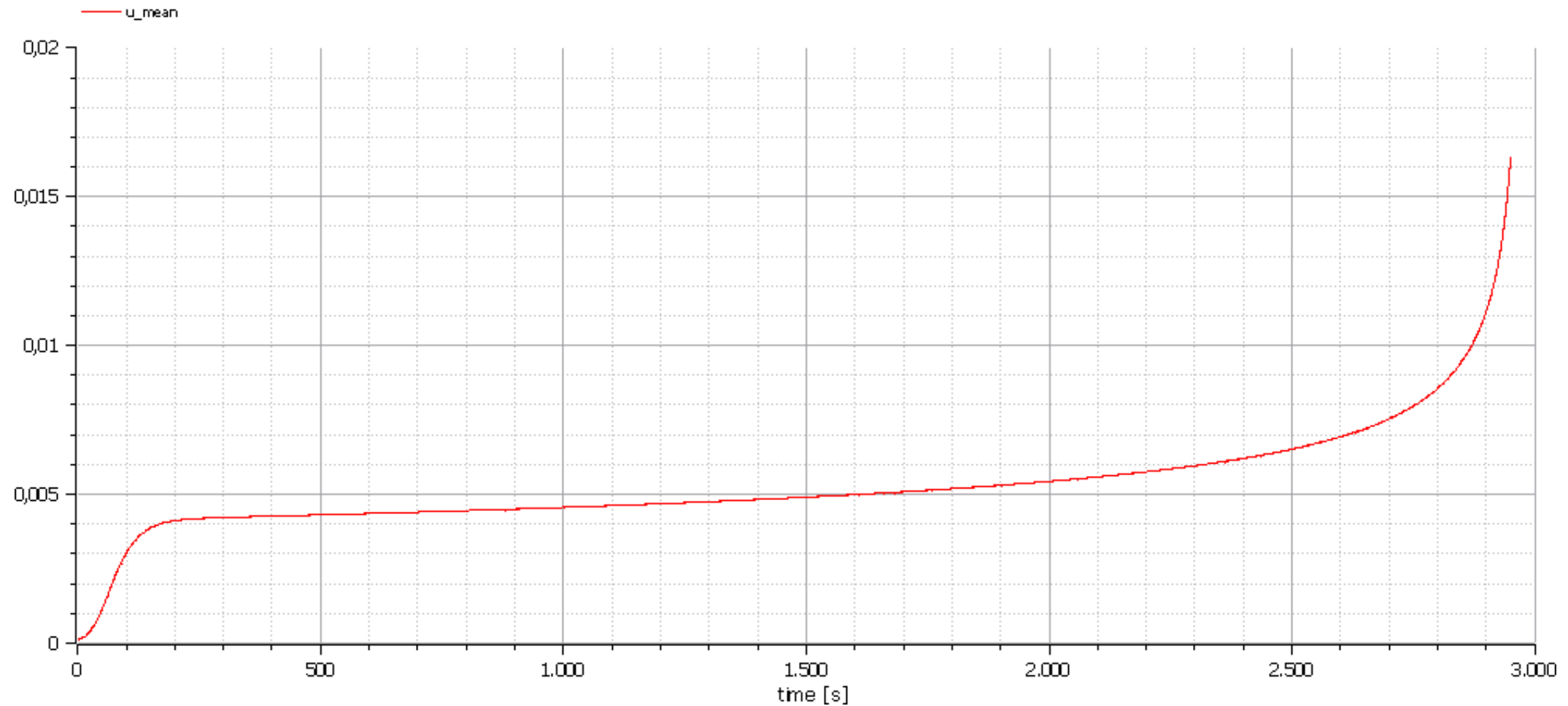
- Density 800 kg/m³
- Yield stress 31.7 Pa
- Oil visc.(newton) 0.22 Pa/s
- Viscosity function values
 - Min 0.22
 - Max 31.7

Simulations – interface tracking.



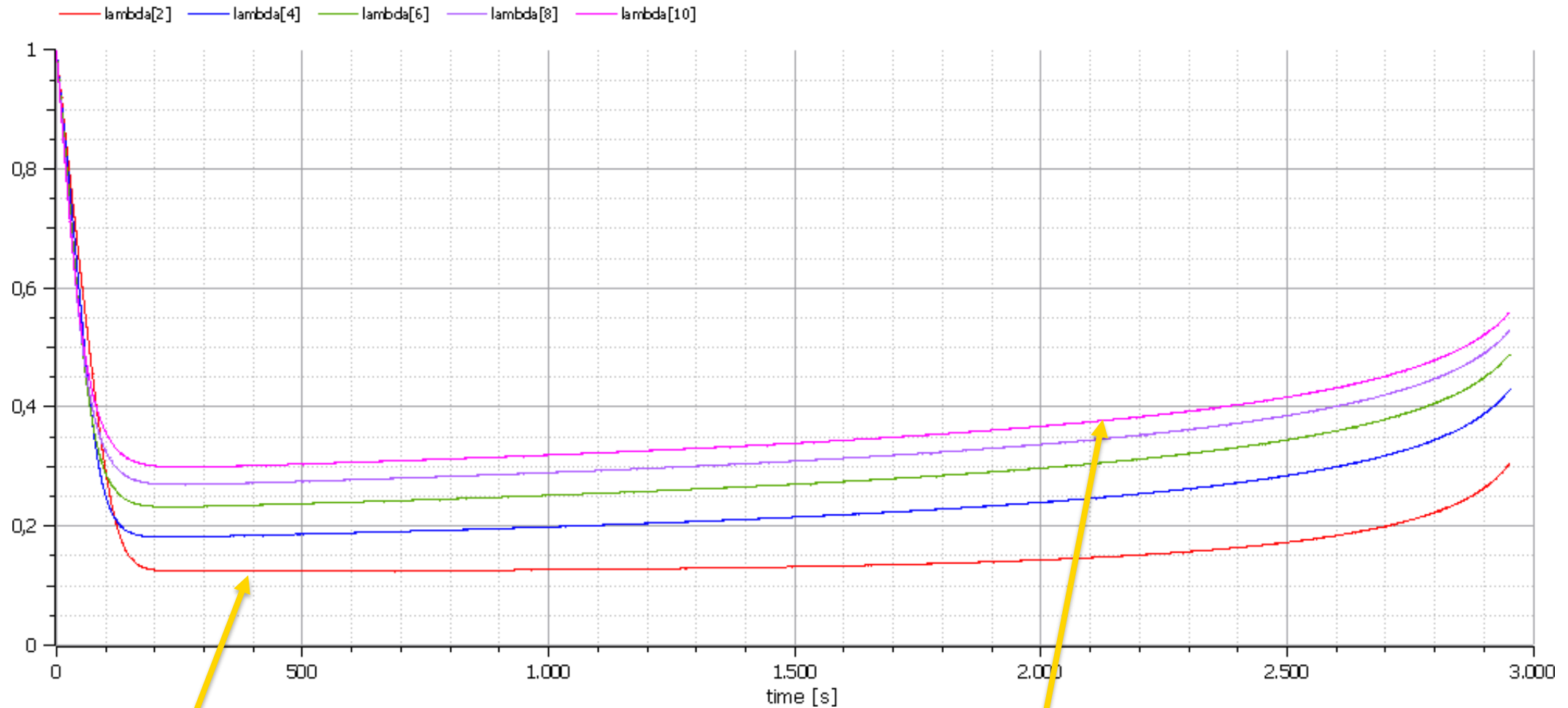
Notice the time: Completely different from experimental observation.

Simulations – interface speed.



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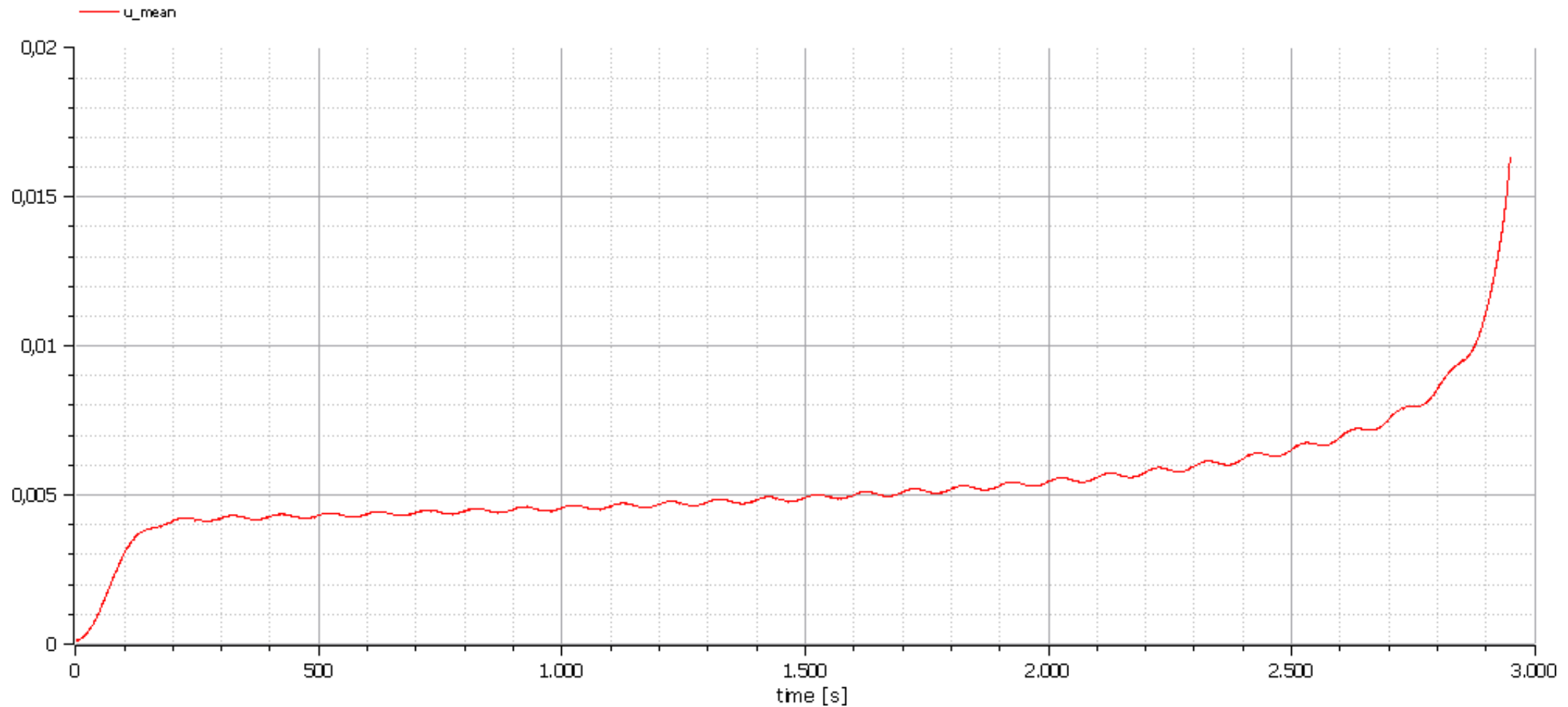
Simulations – interface tracking.



Lambda[2] is close to pipe axis.

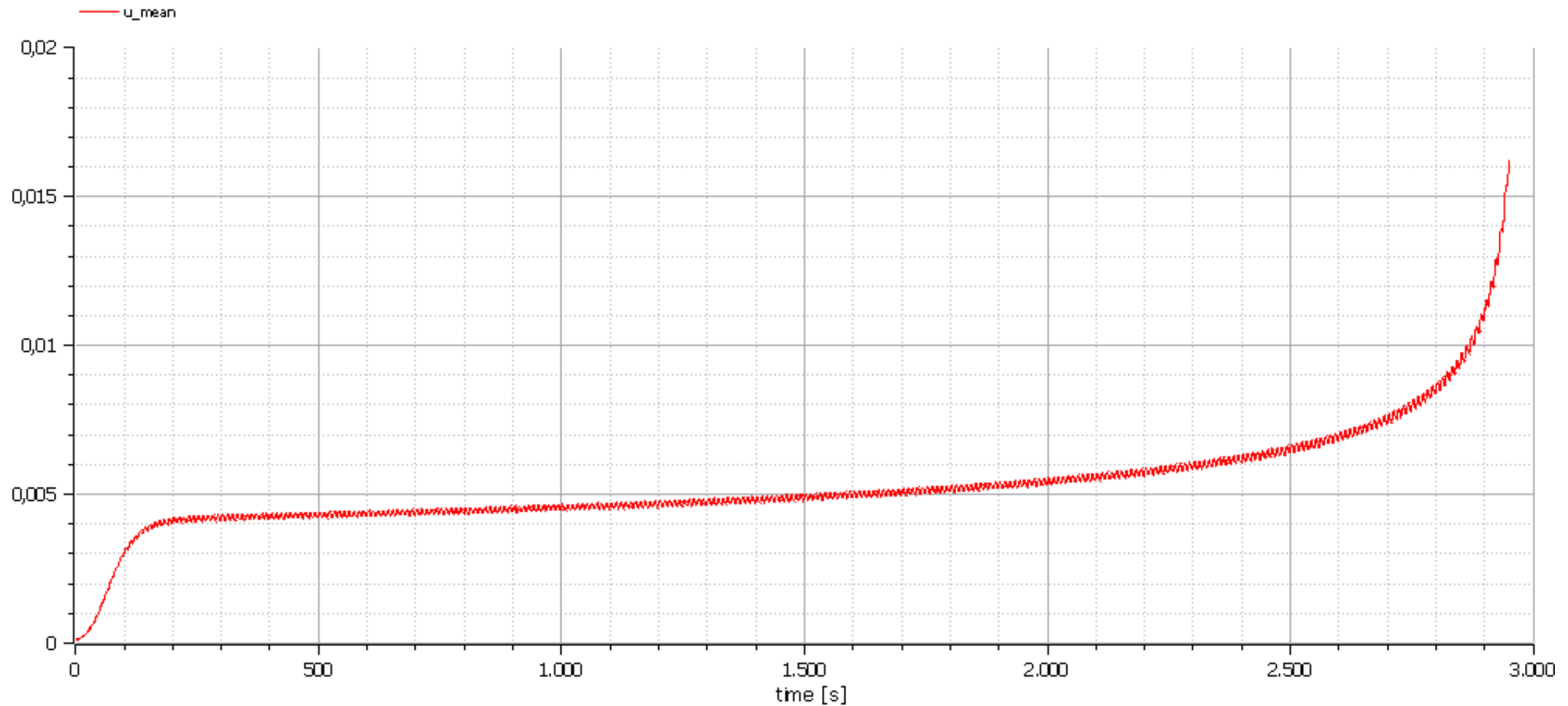
Lambda[10] is close to pipe wall.

Recall Pressure cloud: Simulations – interface speed with inlet pressure oscillations.



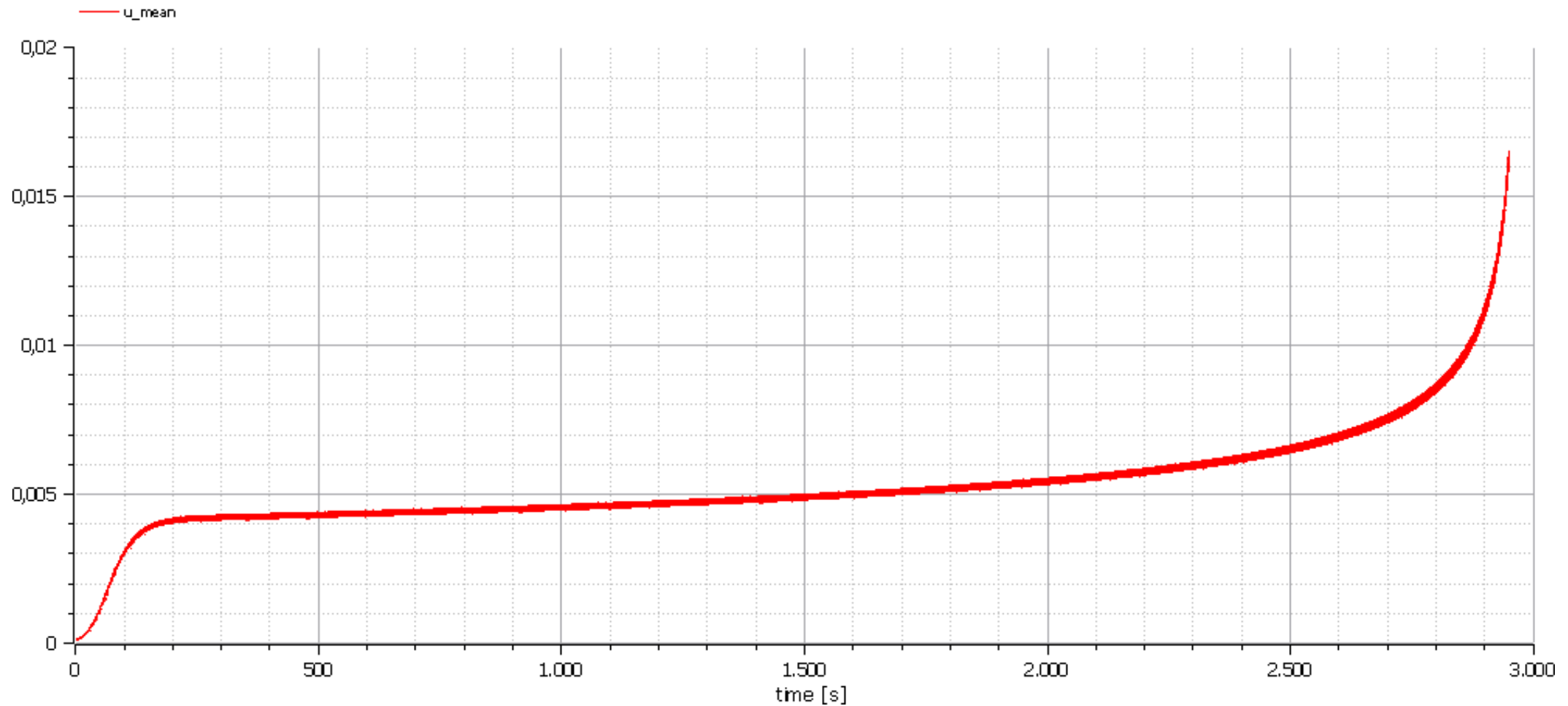
Frequency: 0.01 Hz; sinusoidal; amplitude 0.01 bar

Recall Pressure cloud: Simulations – interface speed with inlet pressure oscillations.



Frequency: 0.10 Hz; sinusoidal; amplitude 0.01 bar

Recall Pressure cloud: Simulations – interface speed with inlet pressure oscillations.



Frequency: 1.00 Hz; sinusoidal; amplitude 0.01 bar

Conclusion.

- Simple thixotropic model from literature has been implemented (in Modelica).
- Experimental outcomes have been analyzed for restart of gelled crude.
- Tuning of the thixotropic model has been performed, however:
 - Time-scale of restart is beyond a factor two!
 - Structure function (Λ) increases towards end of simulation! It should be a memory function, i.e. the longer time the fluid has been stirred then the structure function decrease

Tweaking numerical model-parameters is not sufficient to capture significant physics.

- Modelica has been deployed for model development.
 - A fast tool for ODE/DAE systems development.
 - However, needs special attention of “start-up” conditions
 - (Although not reported here, PDE’s are a completely different story – maybe next time...)

